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Microfluidic doublets in aqueous samples generated by microfabricated thermal probes

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ABSTRACT

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1. Introduction

The ability to manipulate particles is important in several types of biological assays, most notably those involving cells, biomolecules, and bead supports for solid-phase chemistry. Mechanisms for manipulating particle solutions generally fall into two categories: (1) forces which act directly on the particles, and (2) forces imparted on the particles by microflow patterns in the surrounding fluid. The first category includes methods such as optical tweezers [1], dielectrophoresis [2], and optically induced dielectrophoresis [3]. Each of these methods relies on the dielectric properties of the particle. In contrast, the second class of methods is largely independent of the particle's material properties, relying instead on the interaction of the particle with the surrounding fluid. Many of these methods work by generating vortices which trap the particles in a recirculating flow. Microflow patterns can be acoustically generated using out-of-plane [4] or in-plane piezoelectric transducers [5]. When operated at or near the res-

This paper describes an investigation of microfluidic actuation of doublet patterns in samples of water on blank substrates, using singular and arrayed microfabricated thermal probes. A doublet is a twodimensional flow pattern consisting of adjacent, opposing vortices with linear streamlines between them. In this work, each probe consists of a polyimide thin film cantilever with a metal heater near the tip which generates a temperature gradient up to $1 \, ^{\circ}C/\mu m$ along its length. The probes are $360 \, \mu m \log$, $42-120 \, \mu m$ wide, and $3.5 \, \mu m$ thick, and the tips are typically $<1 \, mm$ away from the liquid surface. The velocity of the doublet flow can be controlled by adjusting the temperature of the heat source or by controlling the gap or attack angle between the heat source and the liquid surface. Linear flow velocities exceeding $5 \, mm/s$ and rotational velocities exceeding 1200 rpm are reported.

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onant frequency (typically several 100 kHz), the actuators create ultrasonic standing waves which can trap microscale beads and other particles. Due to the challenges in fabricating mechanical components in planar fabrication processes [6], non-mechanical techniques have also been investigated. For example, an opto-electrostatically driven vortex generated by a focused 50 mW laser spot in combination with a 2 kV/cm electric field was shown to provide a maximum particle velocity of 120 μ m/s in conductive liquids [7]. Vortices driven by electrokinetic instability formed in polymer channels with patterned surface charges [8] operate on a smaller electric field (100 V/cm), but produce slower velocities and require ionic solutions [9]. Pressure differentials and dielectrophoresis [10] are other active methods for generating vortices for particle manipulation.

The Marangoni effect refers to flow on a liquid surface in the presence of surface tension gradients. Due to the inverse relation between surface tension and temperature, Marangoni flow patterns can be deliberately formed by imposing a temperature gradient on the surface [11]. Past approaches have used miniature heaters of various geometries suspended above the fluid layer to generate flow patterns [12,13] in thin layers of oil. In this work, a microfabricated cantilever probe with a sharp linear temperature gradient is used to drive a unique doublet flow in thin films of water.²

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² Portions of this work appear in conference abstract form in [14].



Fig. 1. Schematic of doublet flow generation. A heated thermal probe suspended above a film of water induces a high-speed doublet flow pattern at the surface. The color gradient along the length of the cantilever probe represents a temperature gradient that forms across the cantilever when a current is passed through the microheater.

A fluidic doublet is a two-dimensional flow pattern with streamlines analogous to the field lines in an electric or magnetic dipole. Although rarely observed in nature, doublets can be realized by placing a fluidic sink and source adjacent to one another. Such extraction/injection well pairs have been implemented at very large scales because their mixing characteristics can efficiently purify groundwater [15,16]. Evans [17] and Cola [18] implemented source-sink pairs in microfabricated devices to facilitate advective mixing. A mixing chamber was flanked by channels which either pumped fluid away or into the chamber in a pulsatile fashion. Efficient mixing was demonstrated; however, the devices require mechanical actuation, provided by either integrated [17] or off-chip components [18].

Here, we present experimental evidence that a high speed fluidic doublet, with rotational velocities exceeding 1200 rpm and linear velocities of 5 mm/s, can be realized on a thin aqueous layer placed on a glass slide, without a fluidic chip or pumps. The doublet is driven by a thermal probe suspended above the liquid surface (Fig. 1). Since the probe has no moving parts and makes no contact with the liquid, common problems of mechanical wear, electrode contamination, and bubble generation can be avoided. Additionally, the technique is not restricted to ionic or conductive liquids.

Section 2 introduces the doublet and briefly describes a theoretical model. Section 3 gives experimental results of a typical doublet, and also describes how multiple heat sources (i.e., a thermal probe array) can be superimposed to generate uniform flow.

2. Theoretical

As mentioned above, the doublet is a two-dimensional potential flow consisting of two adjacent vortices of opposing rotational directions, and resulting linear streamlines between them (Fig. 1). It can be expressed in Cartesian coordinates (x, y) by its stream function ψ_D [19]:

$$\psi_D \approx \frac{ma}{\pi} \frac{y}{x^2 + y^2 - a^2} \tag{1}$$

Here, *m* is a constant, and 2a is the separation between the two poles. The product *ma*, also called the dipole moment, reflects the strength of the doublet. The doublet stream function is related to its velocity vector (*u*, *v*) as:

$$u = \frac{d\psi}{dy} = \frac{ma}{\pi} \left(\frac{x^2 - y^2}{\left(x^2 + y^2 - a^2\right)^2} \right)$$
(2)

$$v = -\frac{d\psi}{dx} = \frac{ma}{\pi} \left(\frac{2xy}{\left(x^2 + y^2 - a^2\right)^2} \right)$$
(3)



Fig. 2. Analytical and numerical modeling results for a doublet. (a) Theoretical stream function of an ideal doublet with dipole moment $25 \times 10^{-6} \text{ m}^3/\text{s}$, (b) CFD simulation of doublet flow due to surface momentum 10^{18} kg m/s per m² applied to a $20 \,\mu\text{m} \times 20 \,\mu\text{m}$ region in a two-dimensional fluid layer. The maximum surface velocity vector in this simulation is 200 mm/s.

Fig. 2a illustrates the streamlines for a typical doublet with a dipole moment $25 \times 10^{-6} \text{ m}^3/\text{s}$, which is relevant to the experimental observations described in Section 3.

One way that a doublet flow pattern can be generated on a liquid surface is by adding momentum to a small region on the fluid surface. This is shown in simulations using commercial CFD software (Fluent 6.0, Fluent Corp.). A two-dimensional fluid layer with dimensions $300 \,\mu\text{m} \times 300 \,\mu\text{m}$ is meshed with $2 \,\mu\text{m}$ square elements, and a linear momentum of $10^{18} \,\text{kg m/s}$ per m² is applied to a $20 \,\mu\text{m} \times 20 \,\mu\text{m}$ region in the center of the fluid layer. Under these conditions, doublet flow is observed with scale and geometry similar to the analytical solution above (Fig. 2b). The surface velocity is highest at the center of the doublet, with a maximum velocity of $200 \,\mu\text{m/s}$.

Localized momentum can be imparted to the surface of a liquid via the Marangoni effect. If a directional temperature gradient is imposed on the liquid interface, a corresponding surface tension gradient is also formed due to the inverse relation between surface tension and temperature. Surface stresses result in Marangoni flow oriented from the warm to the cool regions [11,12]. In a typical thermal probe with length 250 μ m, a temperature gradient up to 1 °C/ μ m can be formed along the length of the cantilever. If the probe is positioned near the liquid surface, the temperature gradient is transferred to the surface. Fig. 3 illustrates simulation results where a 360 μ m × 120 μ m × 3 μ m probe with a 7 μ m tall pyramidal tip is suspended 15 μ m above a stationary liquid layer. The sharp, asymmetric gradient produced on the liquid surface (Fig. 3b), which can be controlled by the attack angle of the probe, offers a cause for the forward doublets oriented from the left to right.

3. Experimental

The microfabricated thermal probe consists of a thin film cantilever with a joule heater on the distal end. The probe is fabricated



Fig. 3. (a) Cross-section of a three-dimensional thermal simulation showing a cantilever probe held 15 μ m above the liquid surface. There are 20 equally spaced contours between 306 and 300 K, which is the ambient temperature. (b) Top view of the temperature profile on the liquid surface for 3 different probe attack angles. The maximum surface temperature increase is 0.3 K.

in a 6-step surface micromachining process in which the polyimide cantilever and metal layers are formed on a substrate, released, and subsequently flipped over so that the probe overhangs the silicon substrate [20]. The same process can be used to make a multiprobe array [21]. In this work, two probe geometries are used: R01 (length 360 μ m, width 42 μ m, resistance 25–40 Ω), and R02 (length 360 μ m, width 120 μ m, resistance 20–35 Ω). The probe tip can be heated to 250 °C with <20 mW input power. When heated, a sharp temperature gradient is formed along the length of the probe.

Fig. 4 shows the doublet flow resulting from a thermal probe suspended approximately 20 μ m above the surface of a thin water layer with 15 mW input power. (The air gap between the tip and the sample presents a very large thermal resistance, as noted previously and illustrated in Fig. 3.) Deionized water was spread on a glass slide to the desired depths, typically 50–100 μ m. Due to the evaporation of the water films, the typical duration of the experiments was kept to <10 min. If desired, film evaporation can be minimized by increasing the ambient humidity. Polystyrene beads (diameter 3–10 μ m, Polysciences) were immersed in the water to serve as tracer particles. The time-sequence micrographs, taken at



Fig. 4. High-speed doublet flow is illustrated in 4 sequential micrographs taken at 1/30 s intervals. Polystyrene beads are used to visualize the flow.

1/30 s intervals with a CCD camera, show the movement of the tracers in a high speed, symmetric doublet flow. The maximum flow velocity, measured just to the left of the probe tip, was found to be \sim 5 mm/s. The streamlines and velocities are similar to the analytical model (Fig. 2) which assumes the two poles have a separation $2a = 10 \,\mu\text{m}$ and have a strength $m = 5 \times 10^{-6} \,\text{m}^2/\text{s}$. Based on this, the approximate dipole moment of the experimentally measured doublet is $25 \times 10^{-6} \,\text{m}^3/\text{s}$.

The linear relationship between input power and flow velocity is shown in Fig. 5a. For example, with the cantilever held at a fixed 25 μ m gap above the liquid surface, flow velocities increase by approximately 90 μ m/s for every 1 mW applied, up to a maximum power of 32 mW. Since it is known that the tip temperature increases linearly with input power [20], results show that the flow is proportional to tip temperature.

Reducing the air gap between the probe and the water surface permits the same flow velocities to be achieved at lower levels of input power. For example, extrapolating the results in Fig. 5a suggests that at a 25 μ m gap, one can obtain 5000 μ m/s surface flow velocity by applying 55 mW power to the probe. At a 10 μ m gap, the same velocity can be obtained with only 10 mW power (Fig. 5b). Flow velocities decrease roughly as the inverse square of the air gap. The maximum recorded experimental velocities were obtained at



Fig. 5. Control of flow velocities. (a and b) Peak linear flow velocity as a function of (a) input power, and (b) air gap. (c) Rotation rate in the vortices, as a function of air gap. (d) Flow velocity vs. air gap repeated for three different ambient liquid temperatures. Experimental conditions are shown in each plot. The lines in (a) are a linear fit, and the lines in (b and c) are a fit to $1/x^2$.



Fig. 6. Uniform flow generated with a linear array of doublets. (a) Theoretical streamlines of flow generated by an array of 8 doublets with 85 μ m spacing, obtained by summing the respective stream functions. (b) Linear flow generation using an 8-probe array, numbered 1–8 from the top down. The array was placed 15–20 μ m above the liquid surface, held at a 15° angle, and biased with a total power of 92 mW. Probes 1 and 4 were nonfunctional. Trajectories for 3 particles are marked with a square, triangle, and circle on micrographs taken at 3 s intervals.

air gaps of <10 μ m. Linear velocities of 5000 μ m/s (Fig. 5b) and rotational velocities of 1200 rpm (Fig. 5c) in the adjacent vortices were obtained with 15 mW input power to the probe.

Liquid temperature also plays an important role in determining flow velocities. Cooled liquids generally have larger viscosity and smaller temperature gradients, both of which will reduce Marangoni flow velocities [13]. Fig. 5d shows the consequence of biasing the glass slide below the water sample at 13, 27, and 41 °C using a circulating heating/cooling plate. At each temperature, particle velocities were measured as a function of air gap while holding the probe at constant power and angle. Trends of faster velocities with smaller air gaps hold true as before, but higher liquid temperatures shift the entire trend upward. For example, at a $\approx 10 \,\mu\text{m}$ air gap, the particle velocity at 13 °C is only 165 $\mu\text{m/s}$, compared to nearly 900 $\mu\text{m/s}$ at 41 °C. Overall, particle velocities shown in this figure are slower than the results shown in Fig. 5b due to lower input power levels and the fact that a thinner probe (R01) was used, both of which reduce the surface heat flux.

Complex flow patterns can be generated by forming arrays of doublets using multiple thermal sources. In order to predict the theoretical flow pattern which would arise from multiple doublets, the stream equations for each doublet may be added by applying the principle of superposition. For example, the flow pattern generated by a linear array of 8 doublets with 85 μ m spacing is shown in Fig. 6a. This particular geometry was chosen to model the structure of the multiprobe array. The flow pattern, which resembles a uniform flow channel, was confirmed in experiments. An array of 8 thermal probes [21] was biased at 2.3 V, dissipating 92 mW total power in six probes (probes 1 and 4 were nonfunctional). The resulting flow pattern has a linear flow region with adjacent rotational regions as predicted by simulations (Fig. 6b).

Deviations from uniform flow that were observed in several regions, such as the trajectory marked with a triangle, can be attributed to the difference in air gap between the various probes



Fig. 7. (a) Schematic of subsurface particle flow (80 μ m below the surface). Particles flow radially inward towards the area underneath the microheater tip. Upon reaching this point, they are immediately propelled upwards to the surface. (b) Sequential micrographs show three particles (marked respectively with a square, triangle, and circle) converge towards the center and then disappear from the field of view as they are propelled upwards.

in the array, and the fact that two probes were not operational. The noticeably smaller velocities ($190 \,\mu$ m/s) compared to single probes may be attributed to the smaller temperatures of the heaters in the multiprobe array compared to the single probe. These results illustrate that flow is highly dependent on the geometry of the heat transmitted to the liquid surface. Therefore, it is possible to obtain custom flow patterns by arranging the heat sources in various configurations.

Subsurface particle flow, visualized by focusing the microscope at the bottom of an 80 μ m thick layer of water, differs significantly from the doublet flow patterns observed at the surface. Particles flow radially inward over time, converging on a point directly below the tip of the cantilever. Once at this point, the particles are accelerated upwards toward the surface of the liquid layer (Fig. 7).

4. Discussion and conclusions

This effort has evaluated the doublet flow patterns that are established in films of water when a microfabricated thermal probe is used as the heating element. Linear flow velocities of 5000 μ m/s and rotational velocities up to 1200 rpm are demonstrated using a microfabricated probe at a 10–20 μ m gap and <20 mW input power to the probe. Higher velocities can theoretically be achieved with higher input power to the probe.

The doublet flow pattern can be modeled by local momentum added to the fluid. The momentum, in turn, can be the result of Marangoni stresses caused by a temperature profile imposed on the liquid surface. A directional temperature gradient supplied by the probe evidently leads to the formation of a doublet flow pattern. Although this work has focused on the thermal probes designed in our laboratory [20,21], our results suggest that theoretically, any cantilever structure with a sharp thermal gradient could generate doublet flow. It is notable that a symmetrical, needle-like probe oriented above the water will not produce doublet flow; the asymmetry appears to play an important role in the directionality of flow. There is also some indication that flow direction can be reversed under certain conditions when the probe angle is large. The tendency of water to evaporate may additionally play a role in doublet formation, as the doublet flow pattern is only observed in water, and not in nonvolatile media such as mineral oil. In the long term, models that simultaneously evaluate localized evaporation and Marangoni stresses may help to fully elucidate the microflow patterns. On the experimental side, studies with more complex probe shapes and materials may reveal additional possibilities for this non-contact method of fluidic actuation.

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